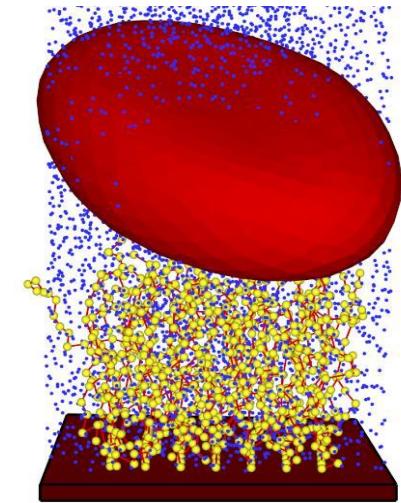
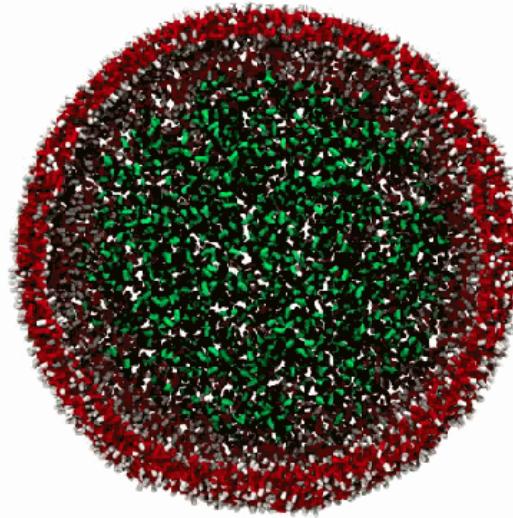
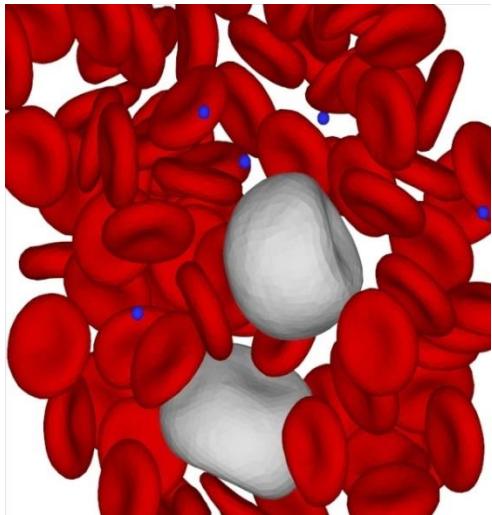


Dissipative Particle Dynamics: Foundation, Evolution and Applications

Lecture 3: New methods beyond traditional DPD



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& Department of Mechanical Engineering, MIT
& Pacific Northwest National Laboratory, CM4

The CRUNCH group: www.cfm.brown.edu/crunch

Outline

1. Single Particle DPD

Particle size: mono-size → multi-size

2. Many-body DPD

Quadratic EOS → Higher-order EOS

3. Energy conserving DPD

Isothermal system → Non-isothermal system

4. Smoothed DPD

Bottom-up approach → Top-down approach

5. Other DPD models

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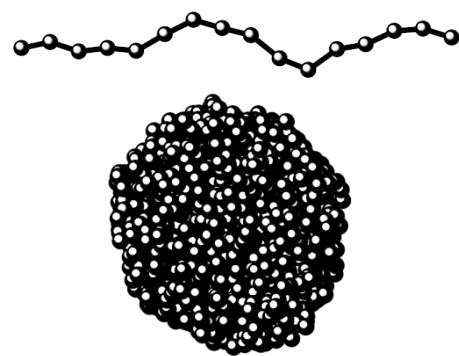
Bottom-up approach → Top-down approach

5. Other DPD models

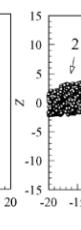
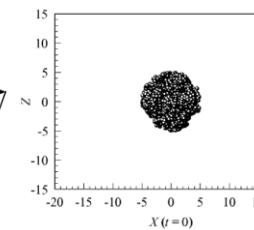
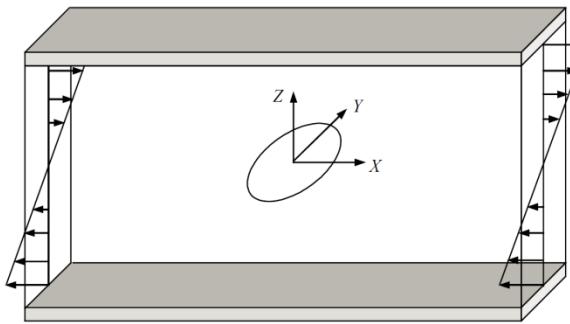
Successful DPD applications using mono-size particles

Application 1: Polymer drops in a shear flow

– Chen, Phan-Thien, Fan & Khoo, J. Non-Newtonian Fluid Mech., 2004.

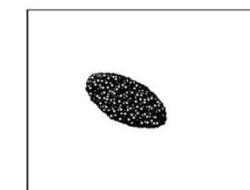


$N = 2096$

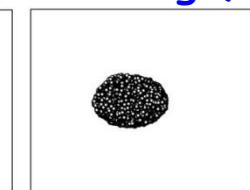


Break-up (low Sc)

Tumbling (high Sc)



$t = 306$



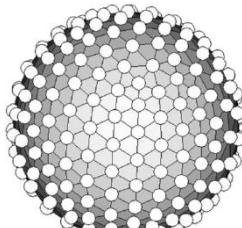
$t = 314$



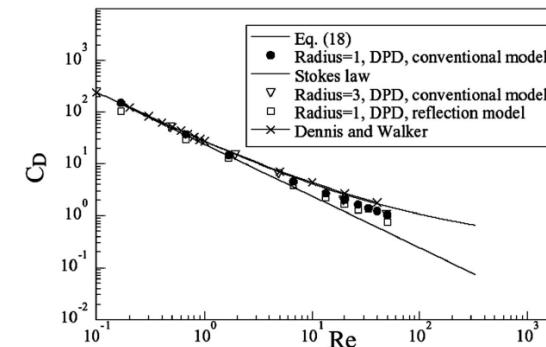
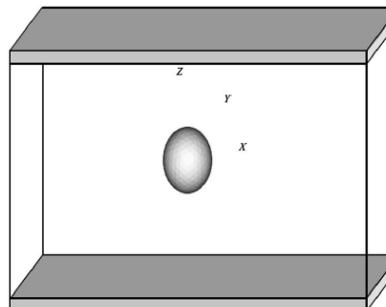
$t = 322$

Application 2: Flow around spheres

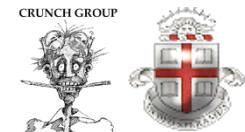
– Chen, Phan-Thien, Khoo & Fan, Phys. Fluids, 2006.



$N = 452$



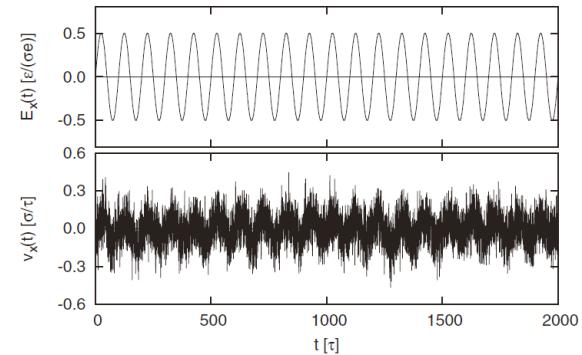
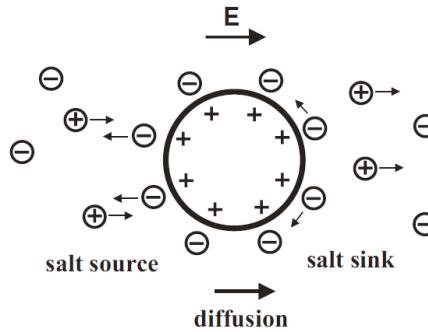
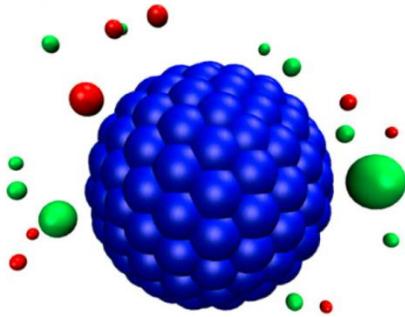
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Successful DPD applications using mono-size particles

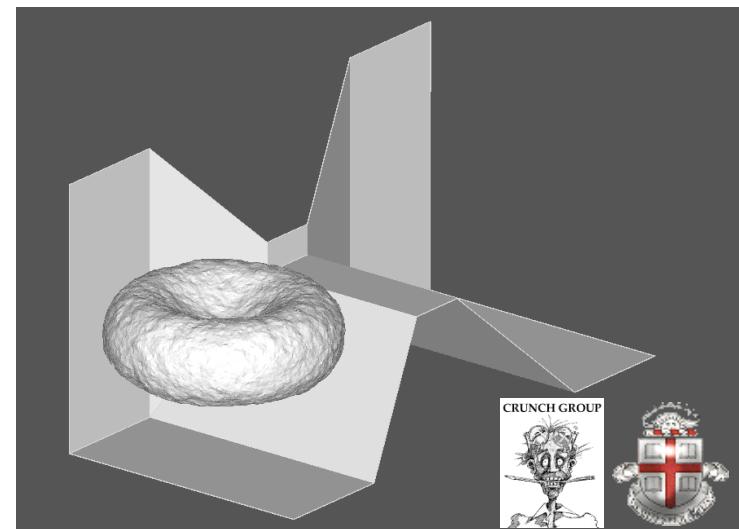
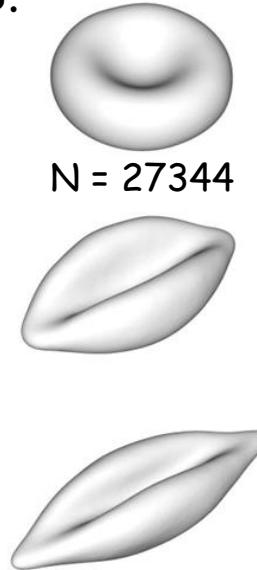
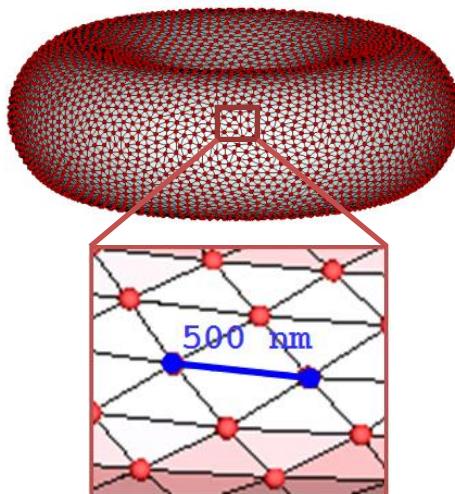
Application 3: Dynamic of colloids in electric fields

— Zhou, Schmitz, Dunweg & Schmid, J Chem. Phys., 2013.



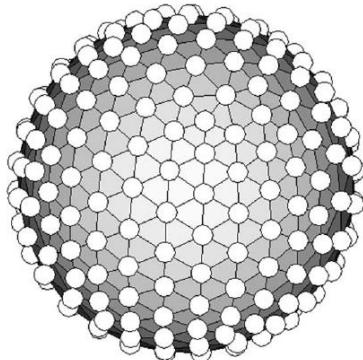
Application 4: Accurate Modeling of Red Blood Cells

— Pivkin & Karniadakis, PRL, 2008.



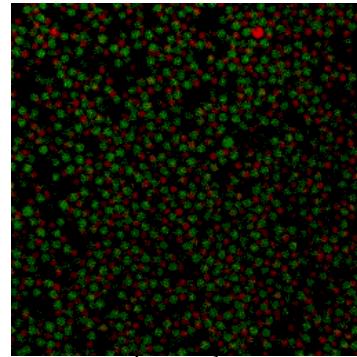
Disadvantage of using mono-size particles

Problem: DPD simulation using mono-size particles is still **too expensive** for some cases such as modeling of many colloids or many RBCs.

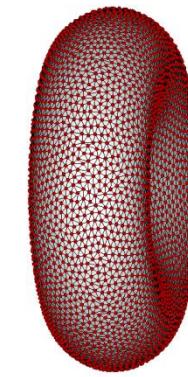


Chen, S., et al., Phys. Fluids, 2006.

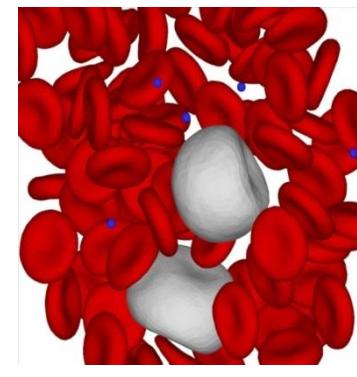
$N = 452$



Many colloids
www.teunvissers.nl



$N = 27344$



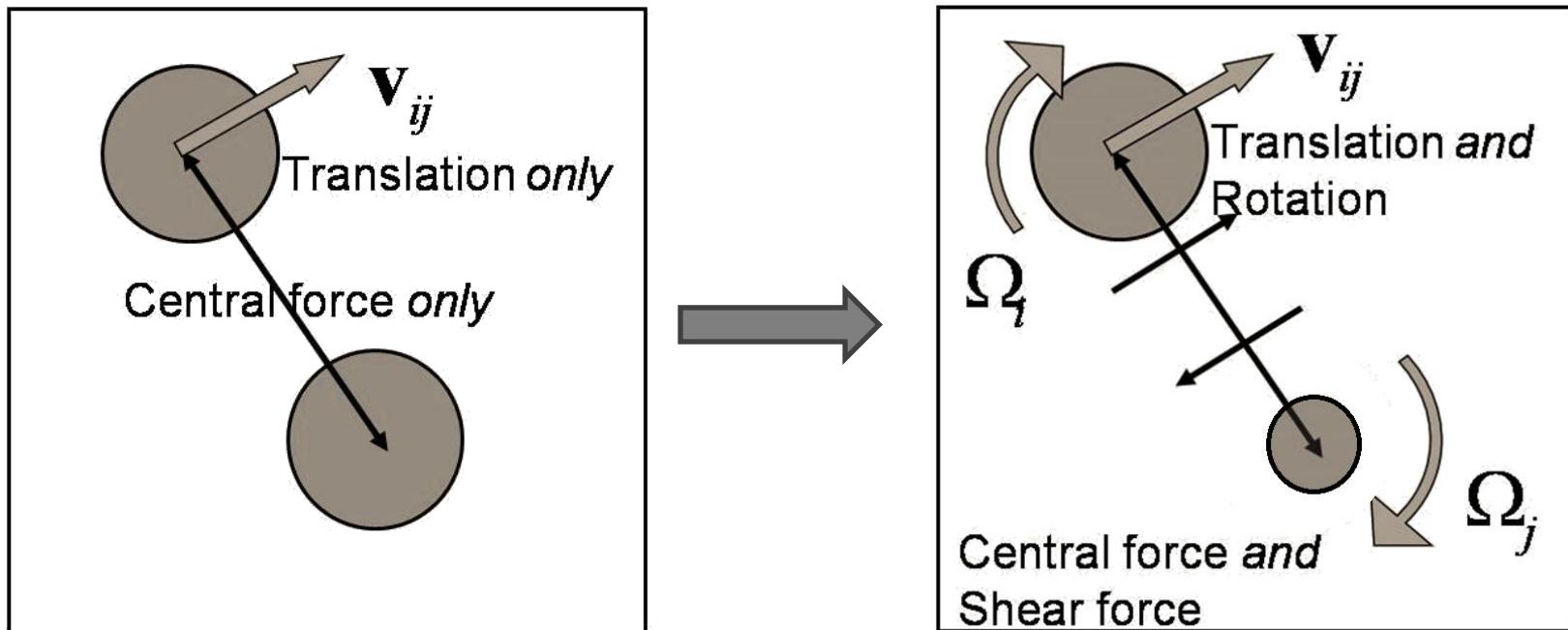
Many RBCs

Solution: Multi-size particles.

— Single Particle DPD model

Single Particle DPD model

DPD Generalization:



Extra requirements:

- ✓ Should be easy to be implemented!
- ✓ Should be a generalization of DPD!

Single Particle DPD model

Equations of Motion:

$$\dot{\mathbf{r}}_i = \mathbf{v}_i$$

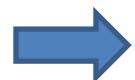
$$\dot{\mathbf{v}}_i = \frac{1}{m} \sum_{j \neq i} \mathbf{F}_{ij}$$

$$\dot{\boldsymbol{\Omega}}_i = \frac{1}{I} \sum_{j \neq i} \mathbf{T}_{ij}$$

$$\mathbf{F}_i = \sum_j \mathbf{F}_{ij}$$

$$\mathbf{T}_i = - \sum_j \lambda_{ij} \mathbf{r}_{ij} \times \mathbf{F}_{ij}$$

$$\lambda_{ij} = \frac{R_i}{R_i + R_j}, \quad \text{and } \lambda_{ij} = 1/2 \quad \text{when } R_i = R_j$$



$$\mathbf{F}_{ij} = \mathbf{F}_{ij}^C + \mathbf{F}_{ij}^T + \mathbf{F}_{ij}^R + \tilde{\mathbf{F}}_{ij}$$

$$\mathbf{F}_{ij}^C = -V'(r_{ij}) \mathbf{e}_{ij} \quad \text{Conservative force}$$

$$\mathbf{F}_{ij}^T = -\gamma_{ij} m \boldsymbol{\Gamma}_{ij} \cdot \mathbf{v}_{ij} \quad \text{Translational force}$$

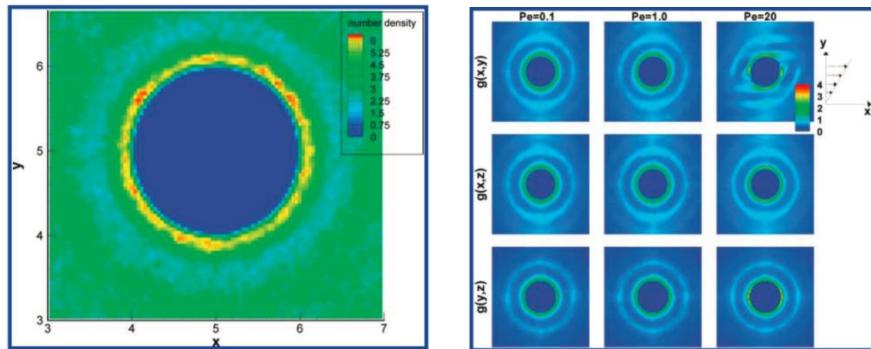
$$\mathbf{F}_{ij}^R = -\gamma_{ij} m \boldsymbol{\Gamma}_{ij} \cdot \left[\mathbf{r}_{ij} \times (\lambda_{ij} \boldsymbol{\Omega}_i + \lambda_{ji} \boldsymbol{\Omega}_j) \right] \quad \text{Rotational force}$$

$$\begin{aligned} \tilde{\mathbf{F}}_{ij} dt &= (2k_B T \gamma_{ij} m)^{1/2} \left[\tilde{A}(r_{ij}) \overline{d\mathbf{W}_{ij}^S} + \right. \\ &\quad \left. \tilde{B}(r_{ij}) \frac{1}{d} \text{tr}[d\mathbf{W}_{ij}] \mathbf{1} + \tilde{C}(r_{ij}) d\mathbf{W}_{ij}^A \right] \cdot \mathbf{e}_{ij} \end{aligned} \quad \text{Random force}$$

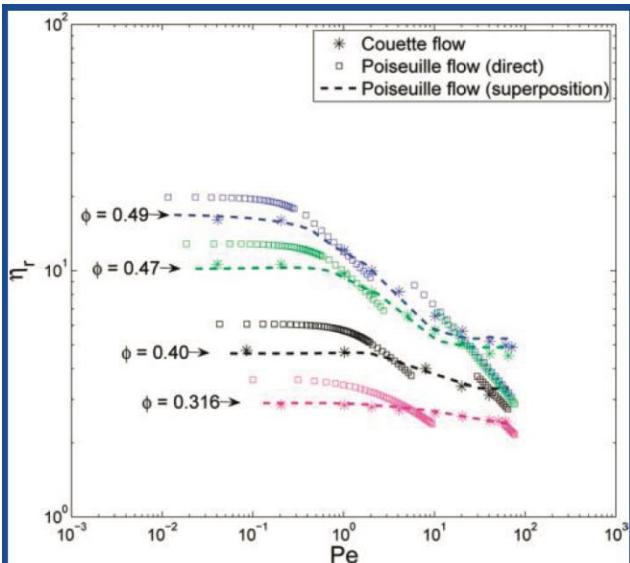
Examples of Single Particle DPD

Rheology in Colloidal Suspensions:

— Pan, Caswell & Karniadakis, Langmuir, 2010.

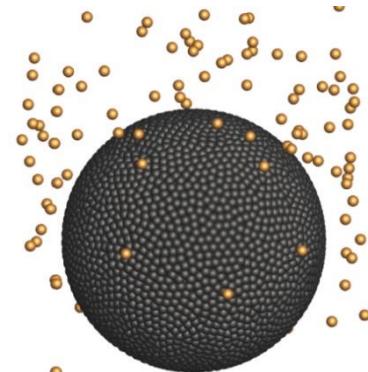


Relative viscosity vs *Pe* number:

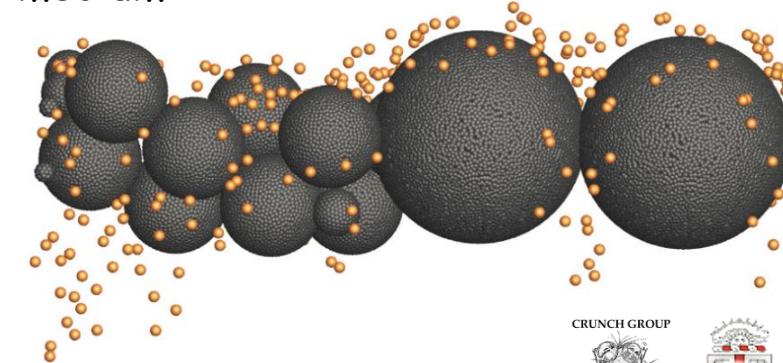


Colloid transport in porous media:

— Pan and Tartakovsky, Adv. Water Resour., 2013.



Colloid transport surrounding a single collector:

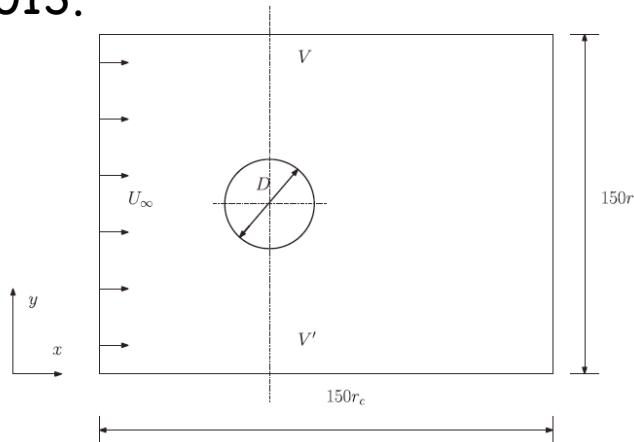


Colloid transport in a polydisperse porous medium:

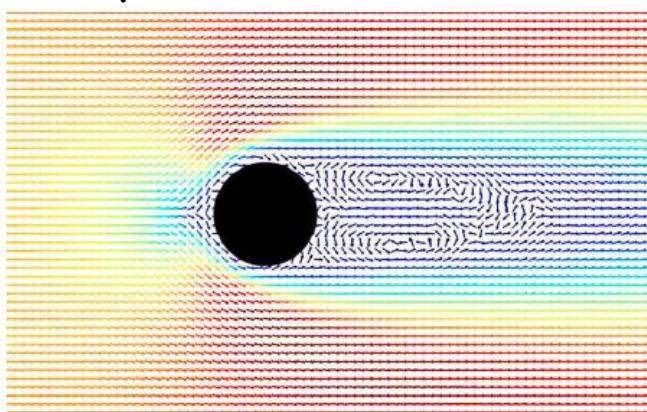
Examples of Single Particle DPD

Flow around a circular cylinder:

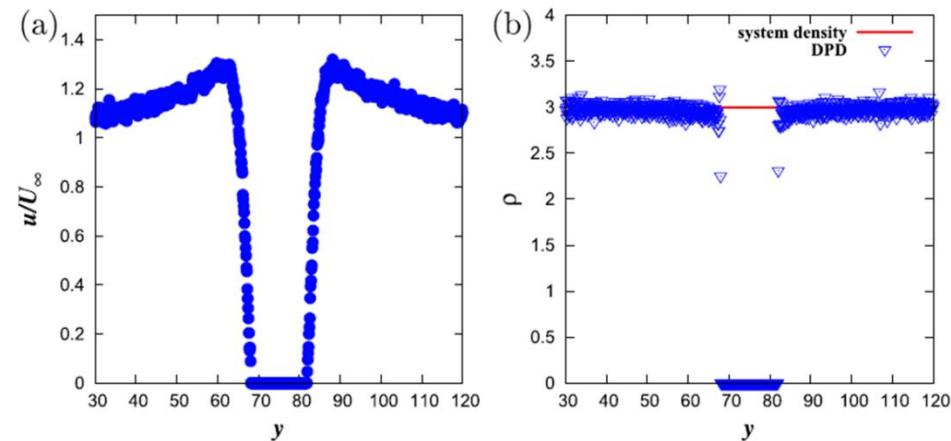
— Ranjith, et al., J. Comput. Phys., 2013.



Velocity vector:



Velocity and density profiles across the cylinder:



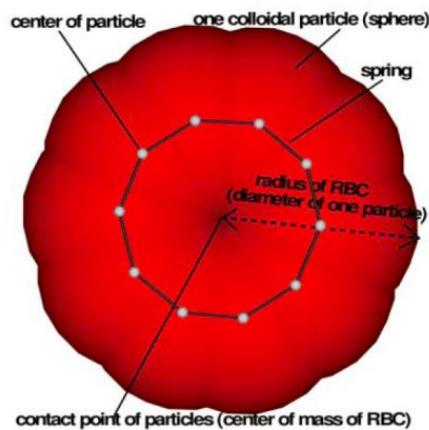
Comparison of drag coefficients:

Re	Experiment	DPD
10	2.93	2.99
20	2.08	2.14
30	1.76	1.74
40	1.58	1.66

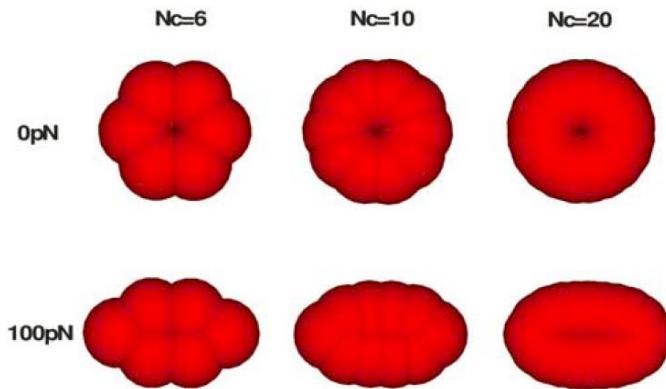


Examples of Single Particle DPD

Low-dimensional model for the red blood cell:

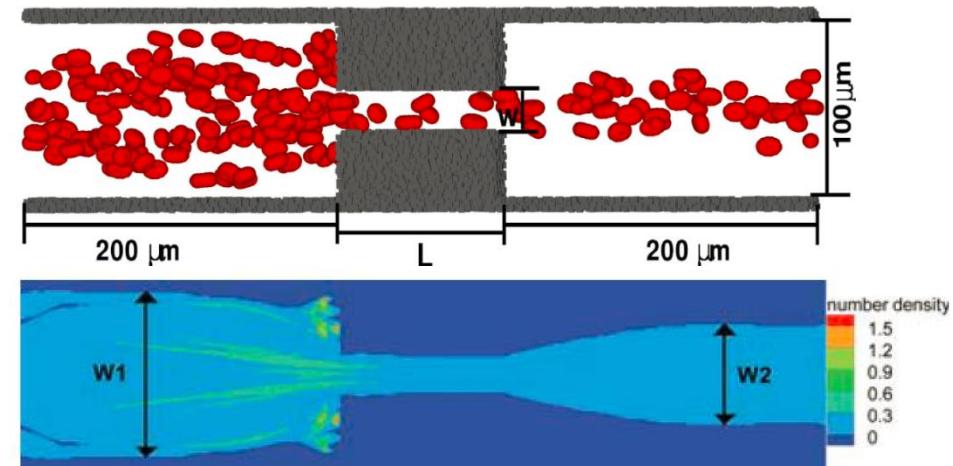


RBC shapes at various stretching forces:



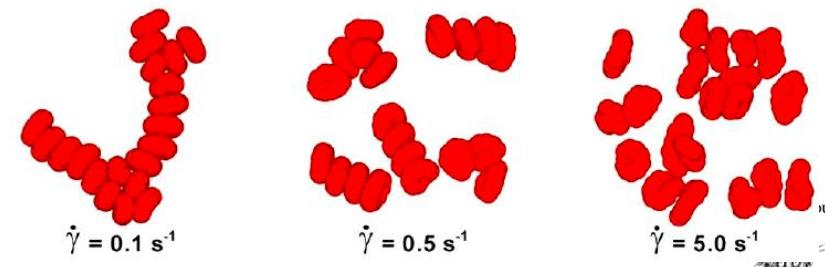
RBCs in a channel with a geometrical constriction:

— Pan, et al., Soft Matter, 2010.



Aggregation of RBCs under shear:

— Fedosov, et al., PNAS, 2011.



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5. Other DPD models

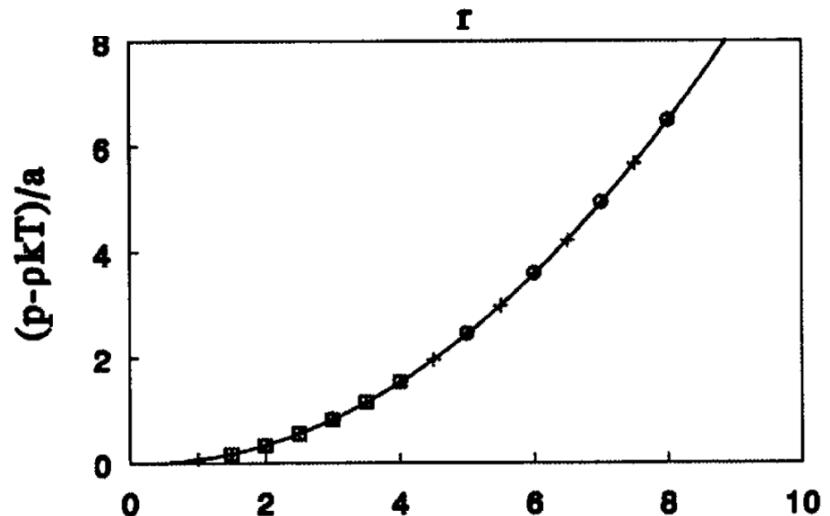
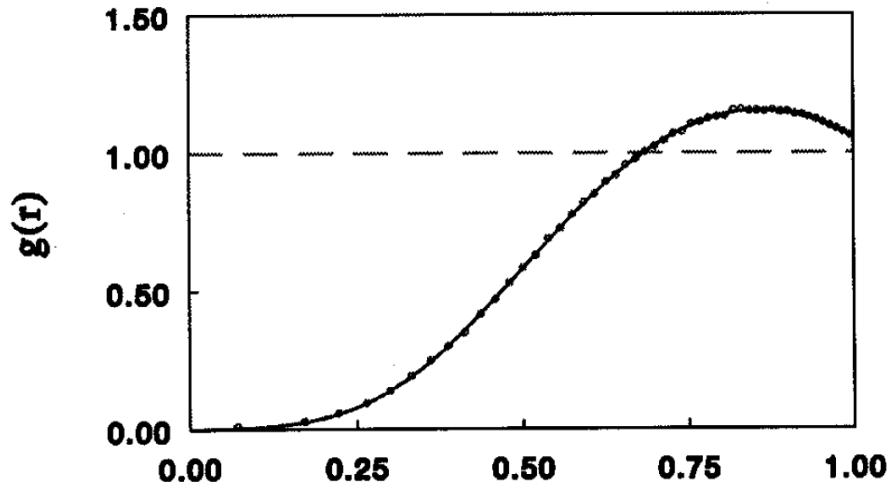
Equation of State (EOS) of traditional DPD

$$\begin{aligned}
 P &= \rho k_B T + \frac{1}{3V} \left\langle \sum_i \mathbf{r}_i \cdot \mathbf{F}_i \right\rangle \\
 &= \rho k_B T + \frac{1}{3V} \left\langle \sum_i \sum_{j>i} \mathbf{r}_{ij} \cdot \mathbf{F}_{ij}^C \right\rangle \\
 &= \rho k_B T + \frac{2\pi}{3} \rho^2 \int_0^1 r F^C(r) g(r) r^2 dr
 \end{aligned}$$



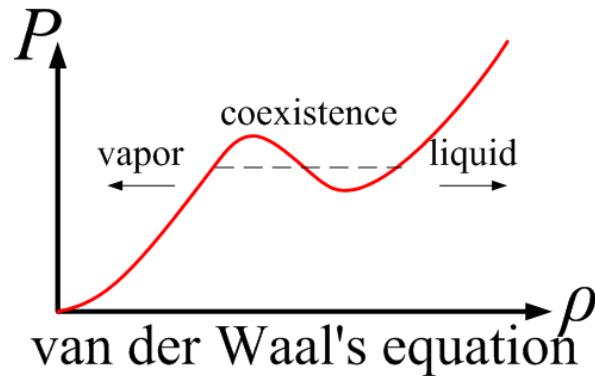
$$F^C(r) = a(1 - r)$$

$$P = \rho k_B T + \lambda \cdot a \rho^2$$



Making conservative force density dependent

The quadratic EOS is monotonic and has no van der Waals loop. It cannot produce liquid-vapor coexistence.



EOS needs high order terms of ρ to model liquid-vapor coexistence.

EOS with high order terms:

	Traditional DPD	Many-body DPD
Force	$\mathbf{F}_{ij}^C = \mathbf{a} \cdot \omega_C(r_{ij}) \mathbf{e}_{ij}$	$\mathbf{F}_{ij}^C = \frac{1}{2} (\mathbf{a}(\rho_i) + \mathbf{a}(\rho_j)) \cdot \omega_C(r_{ij}) \mathbf{e}_{ij}$
EOS	$P = \rho k_B T + \lambda \mathbf{a} \rho^2$	$P = \rho k_B T + \lambda \mathbf{a}(\rho) \rho^2$

– Warren, Phys. Rev. E, 2003.

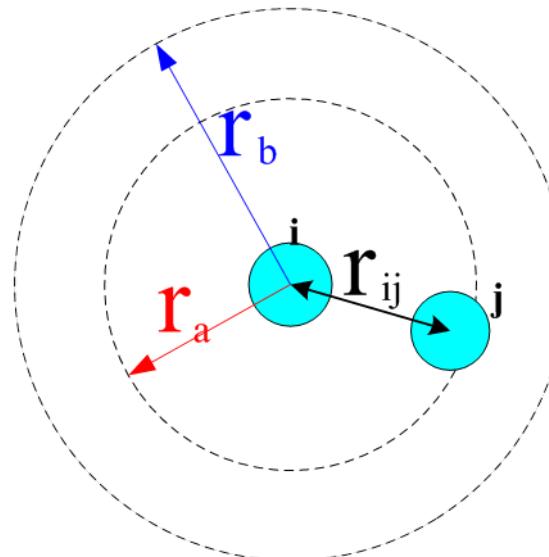
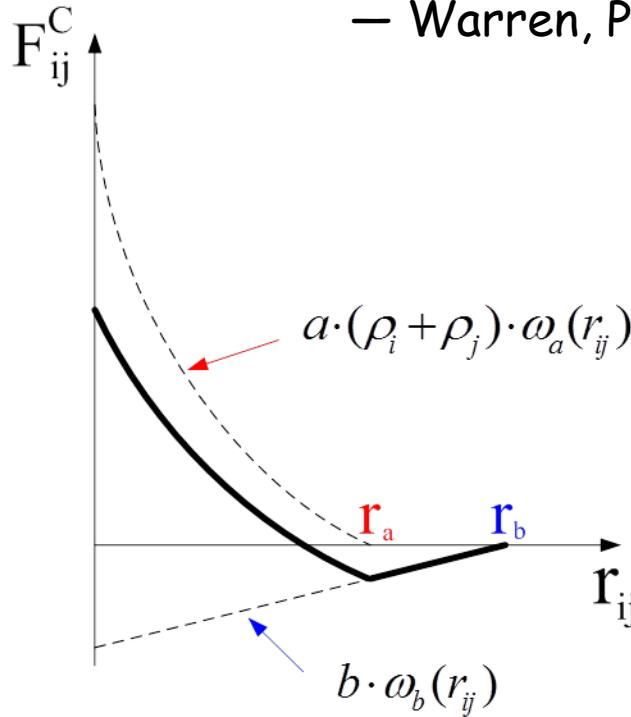
CRUNCH GROUP



Making conservative force density dependent

A common choice: $F_{ij}^C = a \cdot (\rho_i + \rho_j) \cdot \omega_a(r_{ij}) \mathbf{e}_{ij} + b \cdot \omega_b(r_{ij}) \mathbf{e}_{ij}$

– Warren, Phys. Rev. E, 2003.

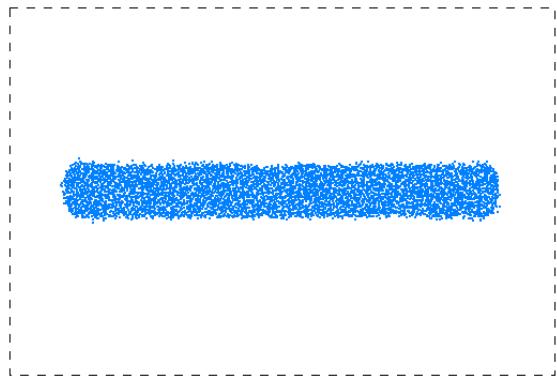


Other approach: $F^C = \nabla \left(k_B T \ln(1 - b \cdot \rho) + a \cdot \rho \right) + \kappa \nabla \nabla^2 \rho$

– Tiwari & Abraham, Phys. Rev. E, 2006.

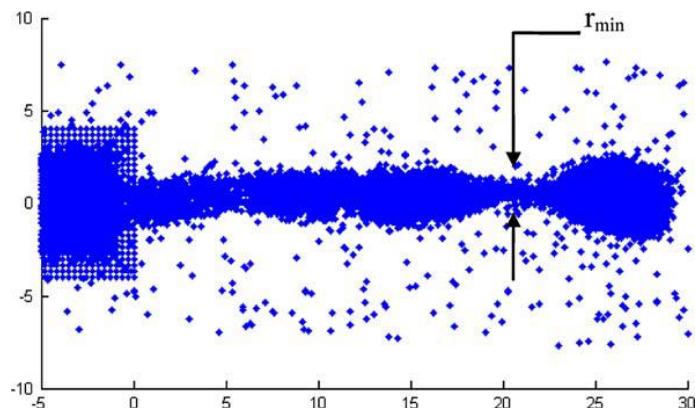
Examples of Many-body DPD

Free oscillation of a droplet:

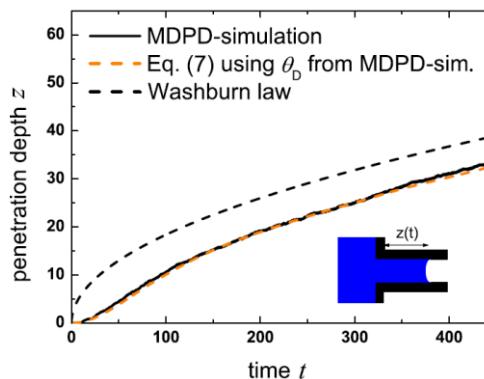


Nano-Jet:

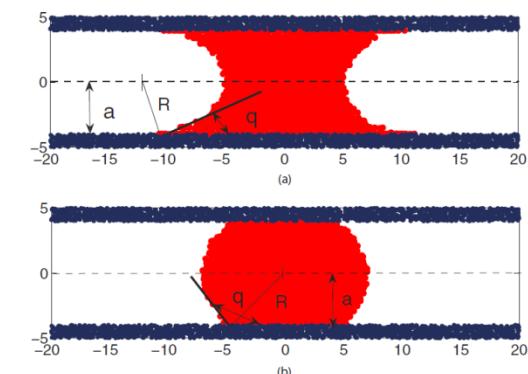
— Tiwari, et al. Microfluid Nanofluid, 2008.



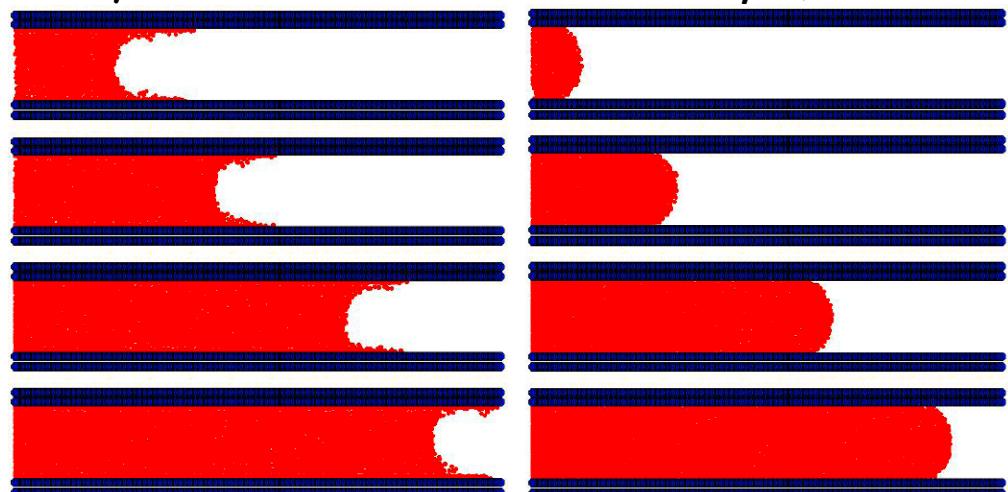
Droplets wetting microchannels:



— Cupelli, et al. New J. Phys., 2008.



— Arrienti, et al., J Chem. Phys., 2011.



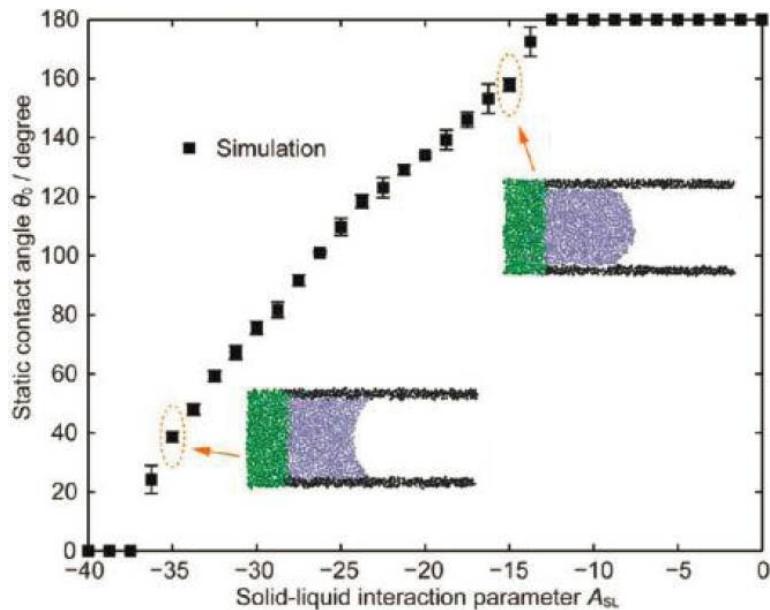
— Pan, W.X., Ph.D Thesis, Brown University, 2010.

Examples of Many-body DPD

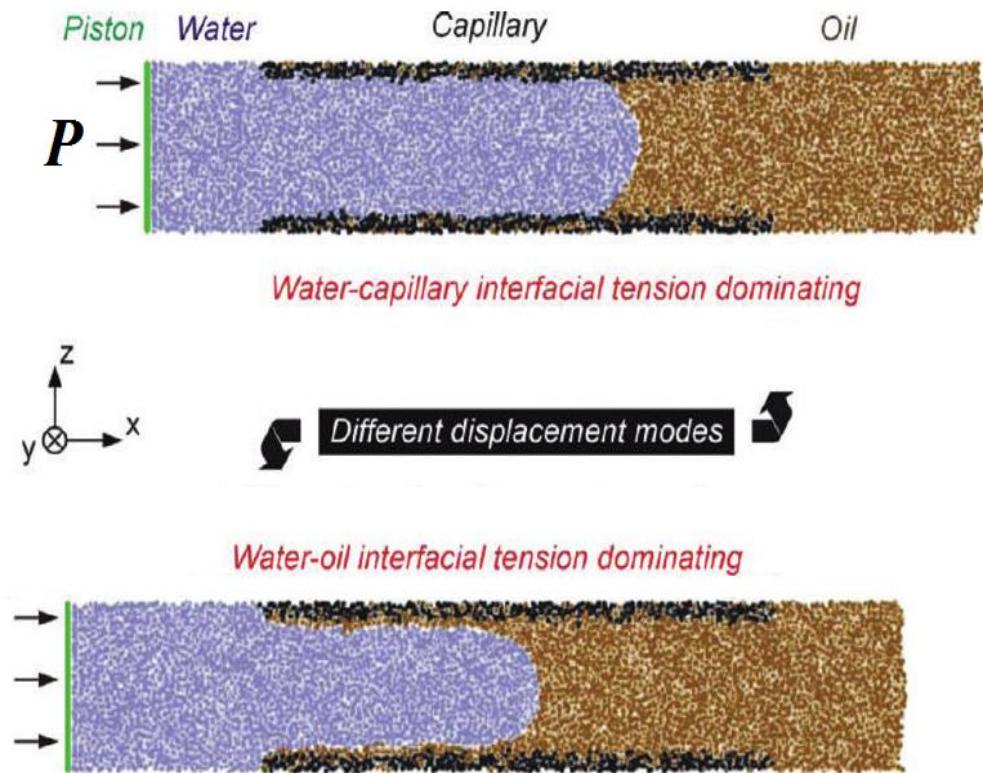
Forced Water-Oil movement in capillary:

— Chen, Zhuang, Li, Dong & Lu, Langmuir, 2012.

Calibration of the solid-liquid interaction parameter A_{SL} related to the static contact angle θ_0 :



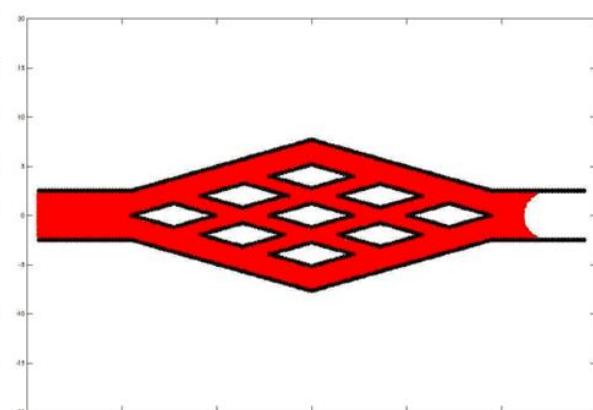
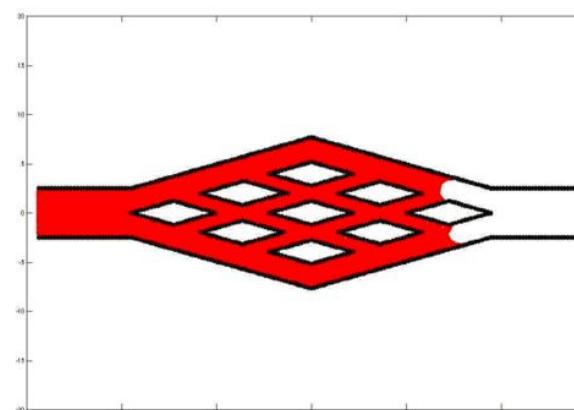
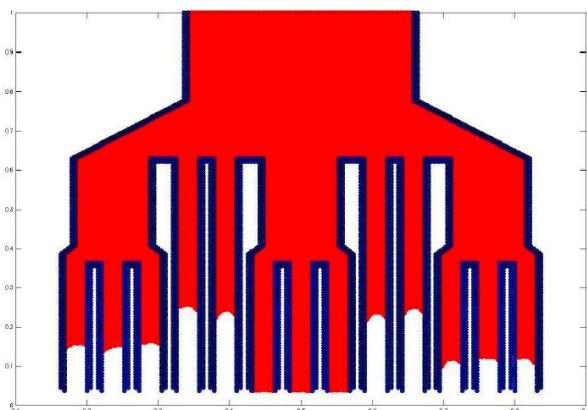
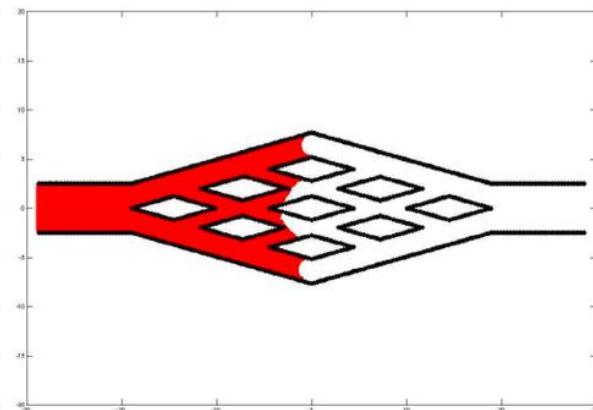
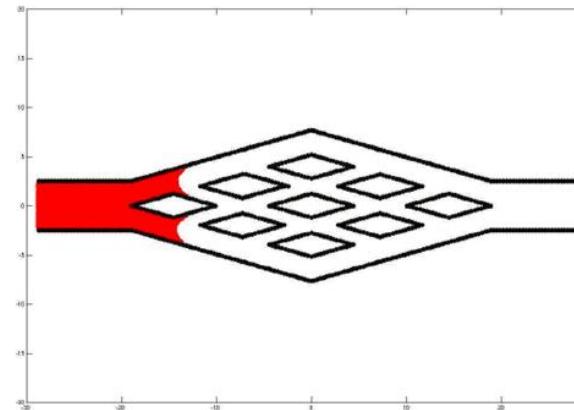
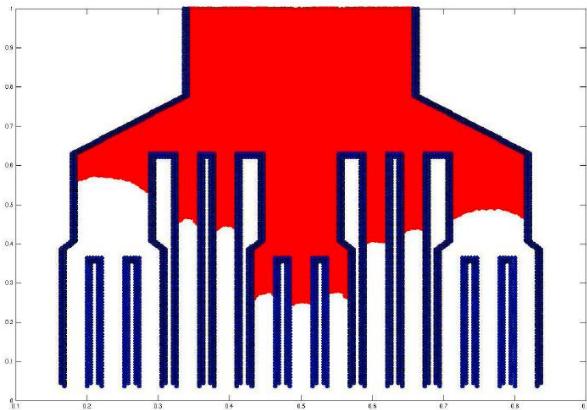
Two different modes of the water-oil displacement:



Examples of Many-body DPD

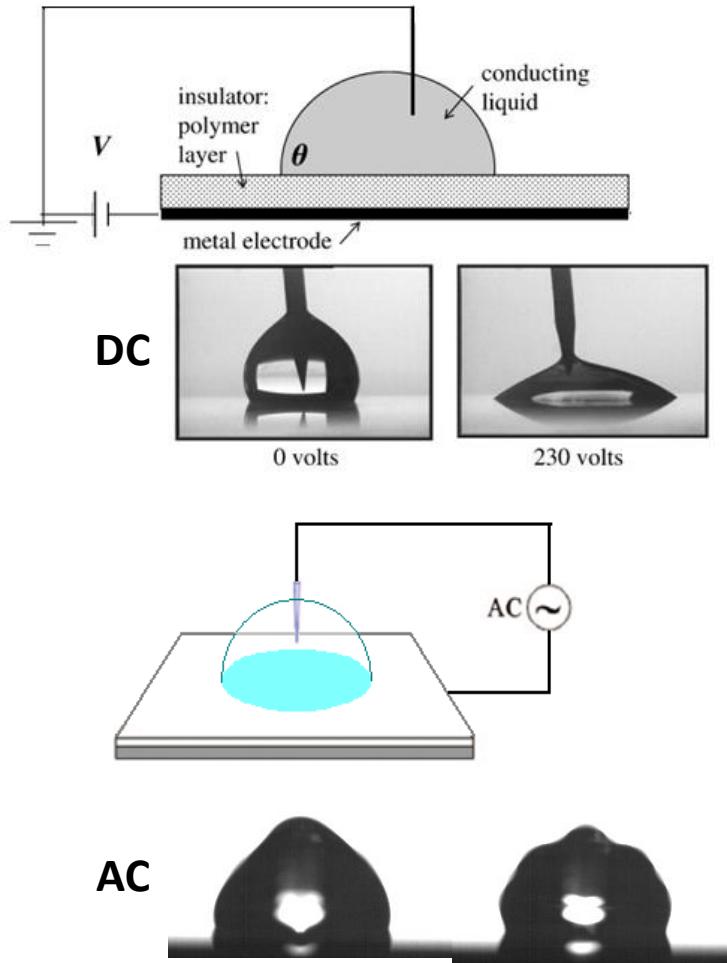
Flow with wetting in microchannel network:

— Pan, W.X., Ph.D Thesis, Brown University. 2010.

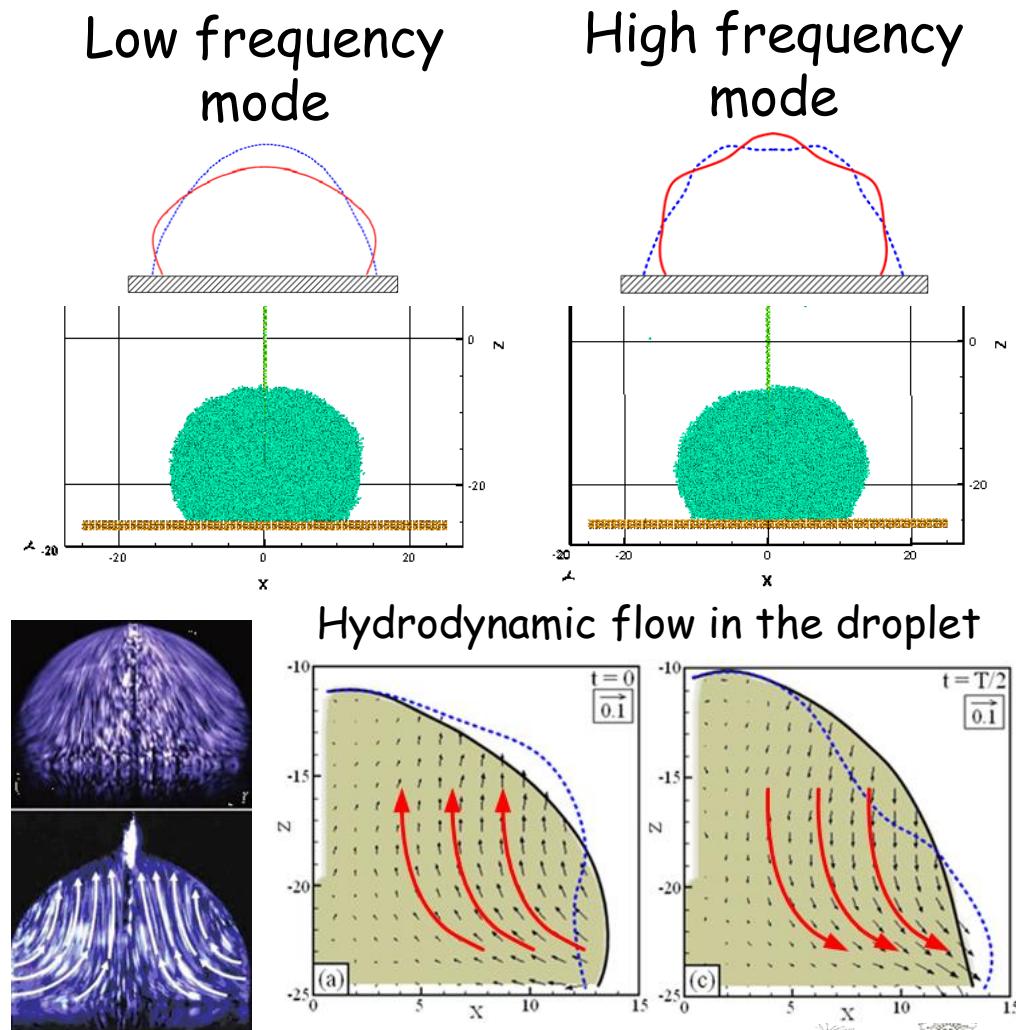


Examples of Many-body DPD

Electrowetting of a droplet:



— Hong et al. J. Micromech. Microeng. 2012.



— Ko, et al., Langmuir, 2008.
— Li, et al., J Adhes. Sci. Technol., 2012.



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5. Other DPD models

Energy is not conserved in traditional DPD

Equations of DPD:

$$\mathbf{F}_{ij}^C = a\omega_C(r_{ij})\mathbf{e}_{ij}$$

$$\omega_C(r) = 1 - r/r_c$$

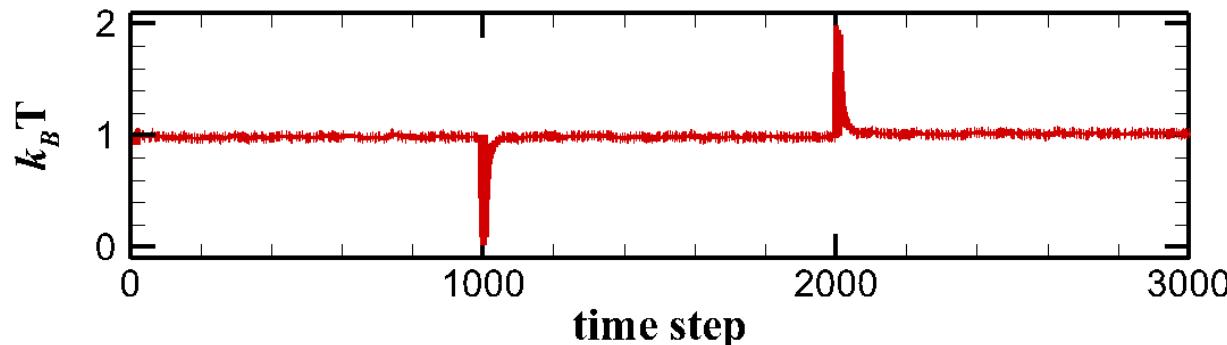
$$\mathbf{F}_{ij}^D = -\gamma\omega_D(r_{ij})(\mathbf{e}_{ij} \cdot \mathbf{v}_{ij})\mathbf{e}_{ij}$$

$$[w_R]^2 = w_D = (1 - r/r_c)^2$$

$$\mathbf{F}_{ij}^R = \sigma\omega_R(r_{ij})\zeta_{ij}dt^{-1/2}\mathbf{e}_{ij}$$

$$\sigma^2 = 2\gamma k_B T$$

DPD thermostat is good to maintain a constant temperature.



Limitation: (no energy equation)

It does not conserve the energy of the system.
Thus, it is only valid for isothermal systems.

Energy-conserving DPD Model for non-isothermal fluid systems

Include the energy equation:

$$\mathbf{F}_{ij}^C = \alpha \omega^C(r_{ij}) \mathbf{e}_{ij}$$

$$\mathbf{F}_{ij}^D = -\gamma \omega^D(r_{ij}) (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}$$

$$\mathbf{F}_{ij}^R = \sigma \omega^R(r_{ij}) \zeta_{ij} dt^{-1/2} \mathbf{e}_{ij}$$

$$\omega^C(r) = 1 - r / r_c$$

$$[w_R]^2 = w_D = \left(1 - \frac{r}{r_c}\right)^S$$

$$\sigma_{ij}^2 = \frac{4\gamma_{ij} k_B T_i \cdot T_j}{T_i + T_j}$$

– Ripoll & Español, Int. J. Mod. Phys. C, 1998.

$$C_v dT_i = \sum_{i \neq j} q_{ij}^{cond} dt + \sum_{i \neq j} q_{ij}^{visc} dt + \sum_{i \neq j} q_{ij}^R dt$$

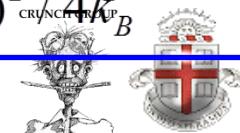
$$q_{lj}^{cond} = \sum_{j \neq i} k_{ij} w_{CT}(r_{ij}) \left(\frac{1}{T_i} - \frac{1}{T_j} \right) \quad \text{Heat conduction}$$

$$q_{lj}^{visc} = \frac{1}{2C_v} \sum_{j \neq i} \left(w_D(r_{ij}) \left[\gamma_{ij} (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij})^2 - \frac{(\sigma_{ij})^2}{m} \right] - \sigma_{ij} w_R(r_{ij}) (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \zeta_{ij} \right) \quad \text{Viscous heating}$$

$$q_{lj}^R = \sum_{j \neq i} \alpha_{ij} w_{RT}(r_{ij}) dt^{-1/2} \zeta_{ij}^e \quad \text{Fluctuating term}$$

$$w_{CT}(r_{ij}) = [w_{RT}(r_{ij})]^2 = \left(1 - \frac{r_{ij}}{r_{cut}}\right)^{S_T}$$

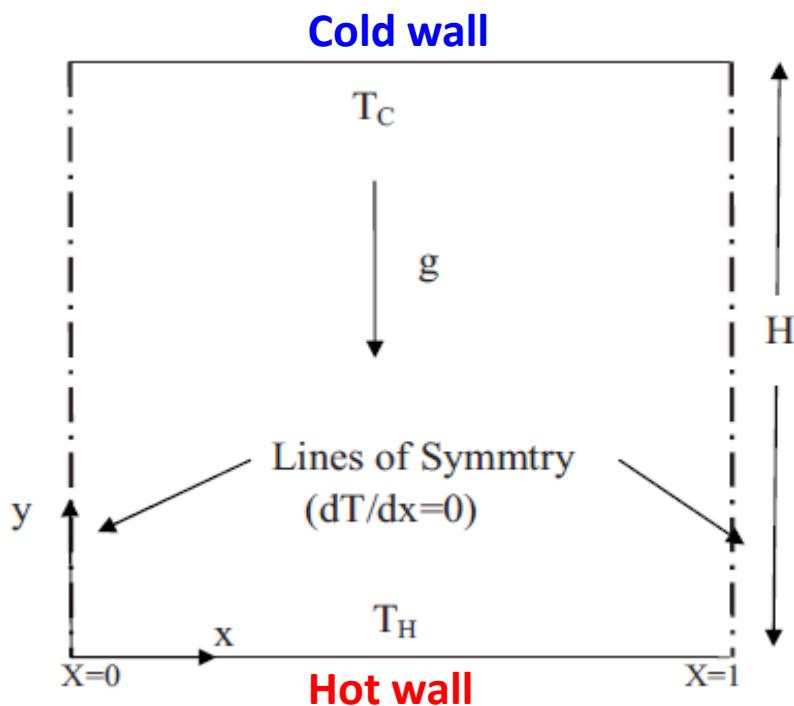
$$\alpha_{ij} = \sqrt{2k_B k_{ij}}, \quad k_{ij} = C_v^2 \kappa (T_i + T_j)^2 / 4k_B$$



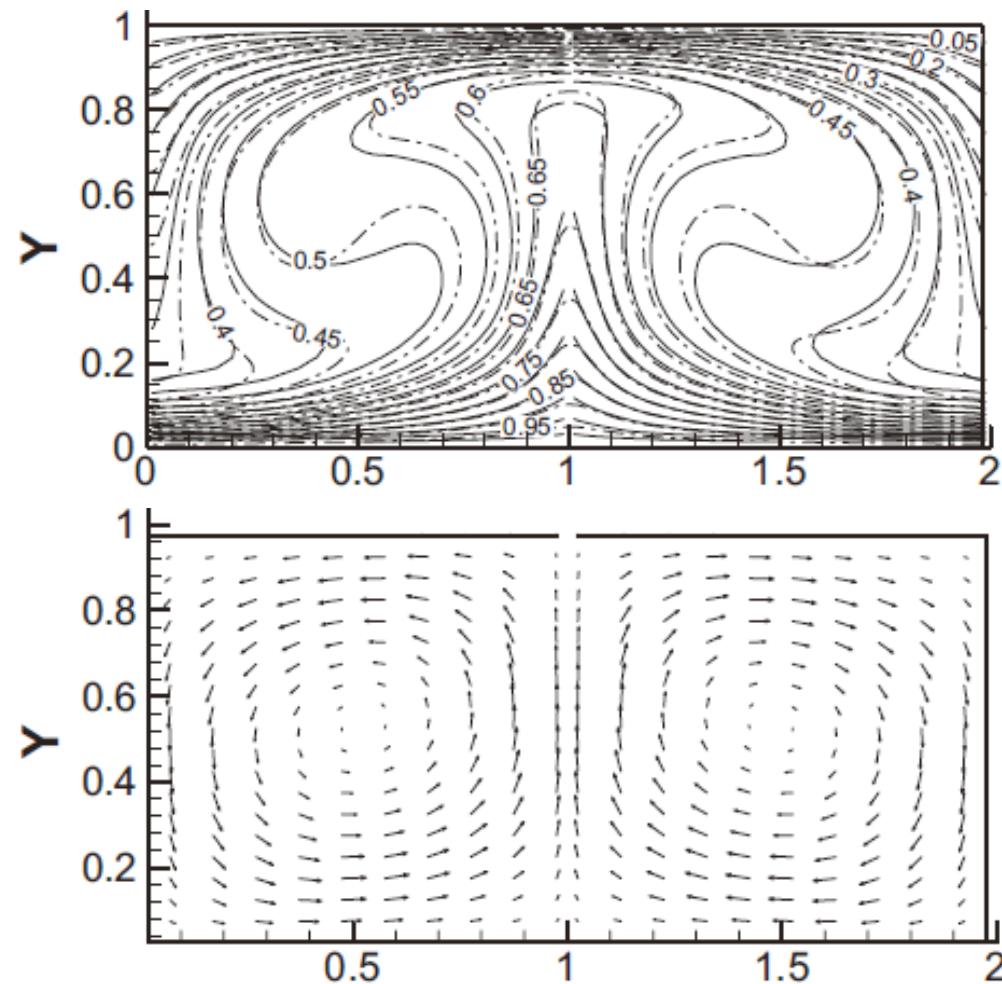
Examples of Energy-conserving DPD

Natural convection heat transfer simulation:

— Abu-Nada, E., Phys. Rev. E, 2010.



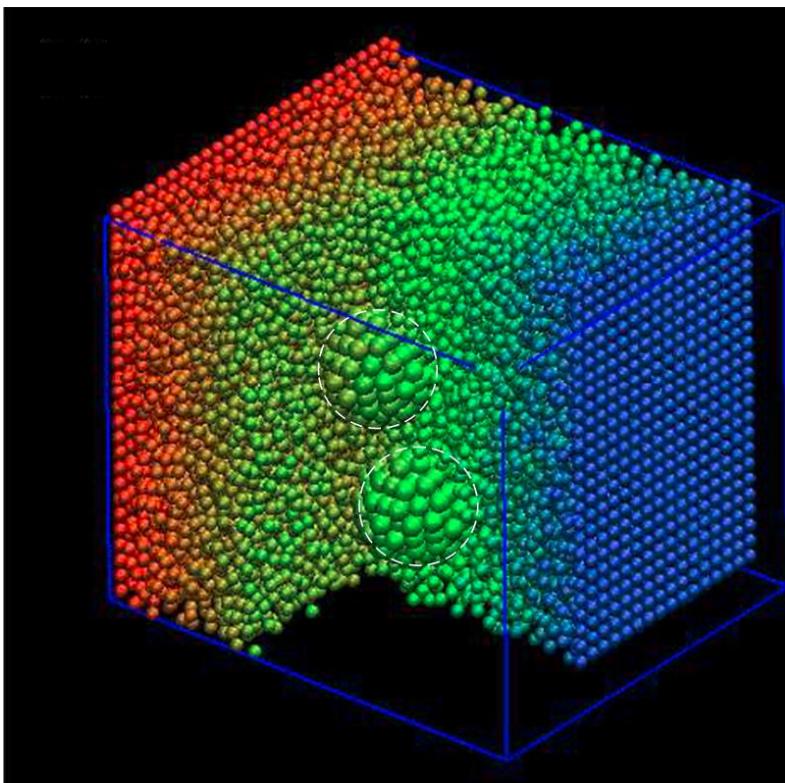
Temperature isotherms and velocity field (solid lines: eDPD, dashed dotted lines: finite volume solutions):



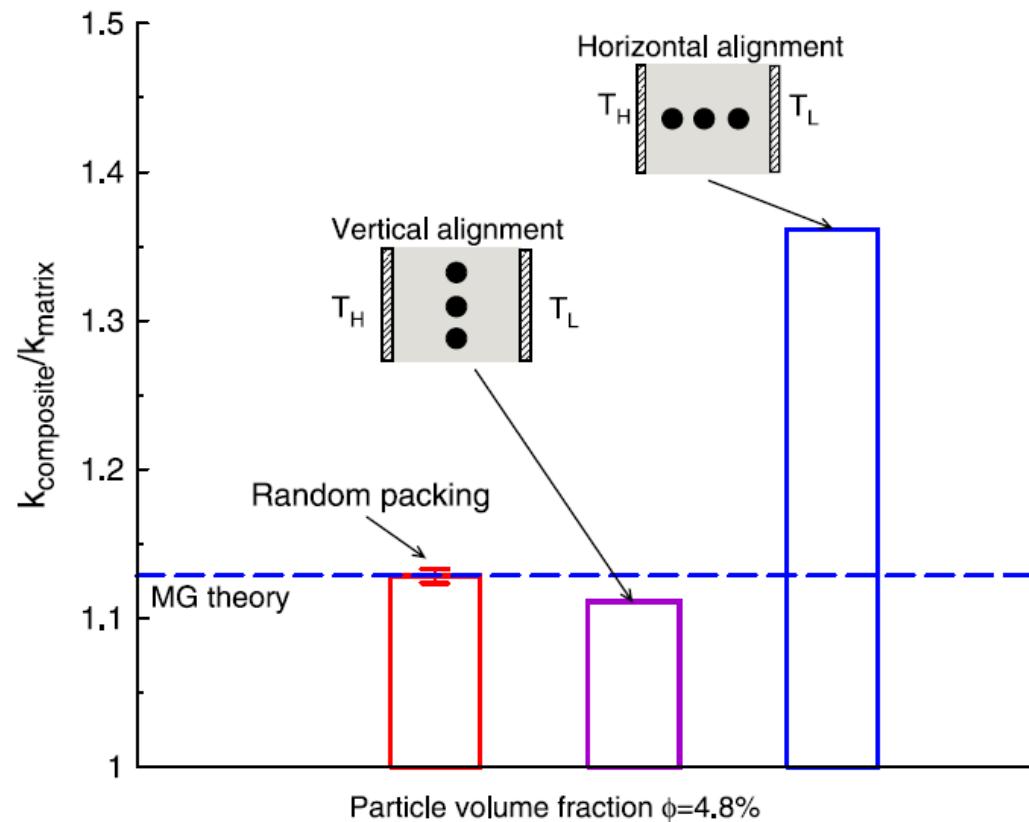
Examples of Energy-conserving DPD

Heat conduction in nanocomposite:

— Qiao and He, Molecular Simulation, 2007.



Thermal conductivity enhancement by nanoparticles:

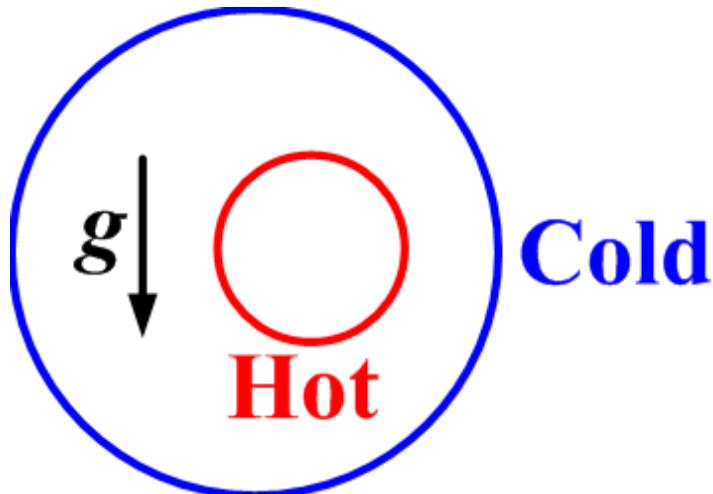


Examples of Energy-conserving DPD

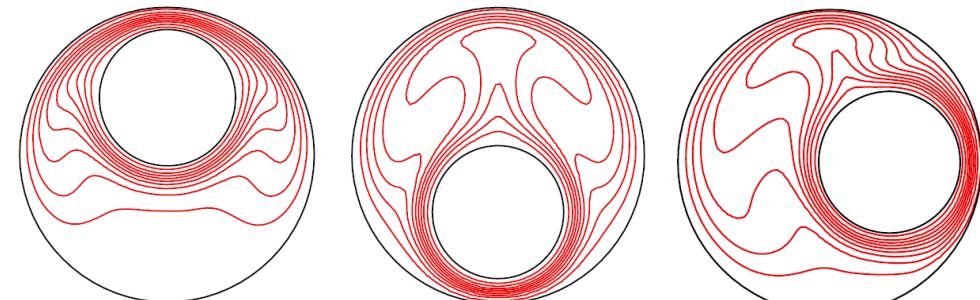
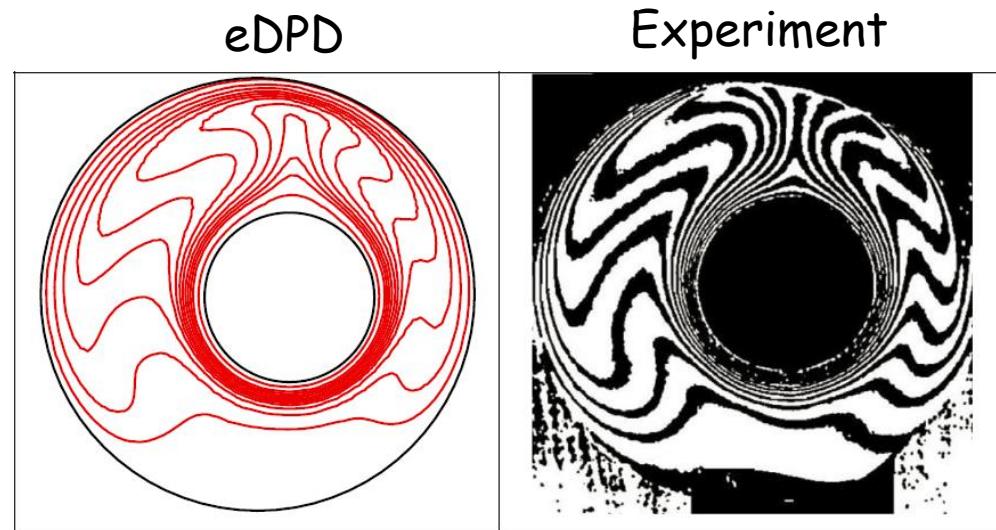
Natural convection in eccentric annulus:

— Cao, et al., Int. J. Heat Mass Transfer, 2013.

Physical model:



Isotherms for $Ra = 4.59 \times 10^4$ and $Pr = 0.7$:

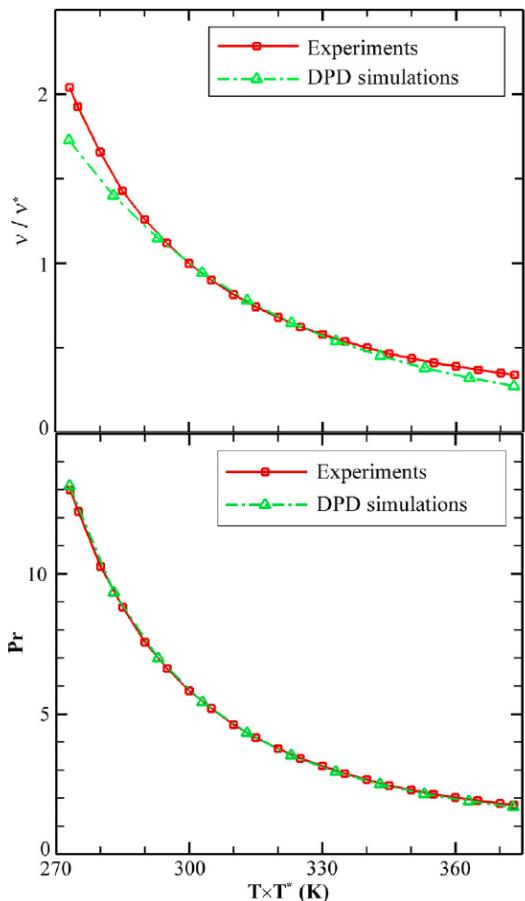


Examples of Energy-conserving DPD

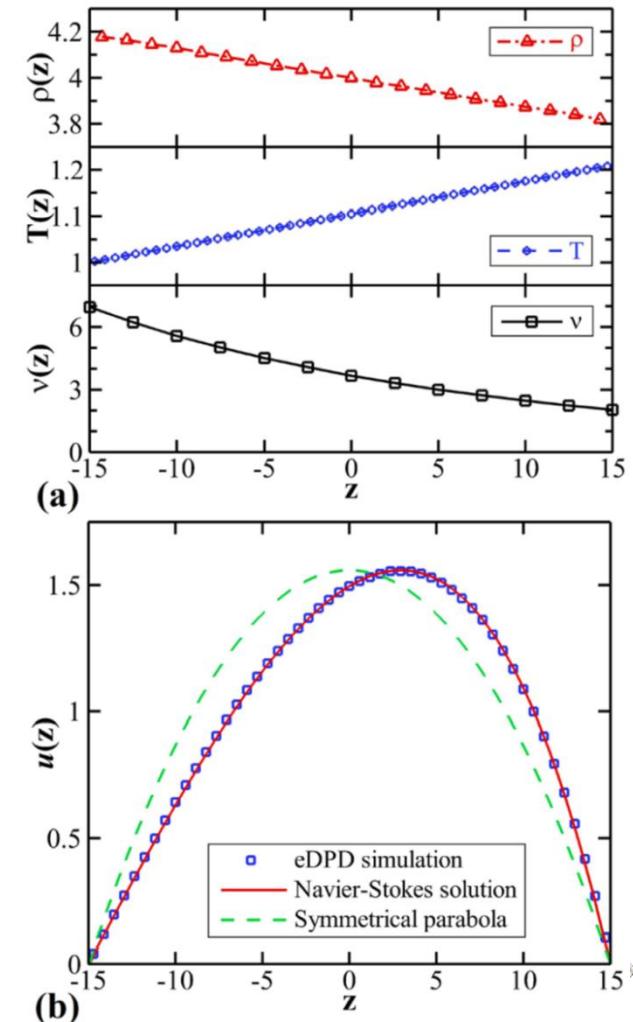
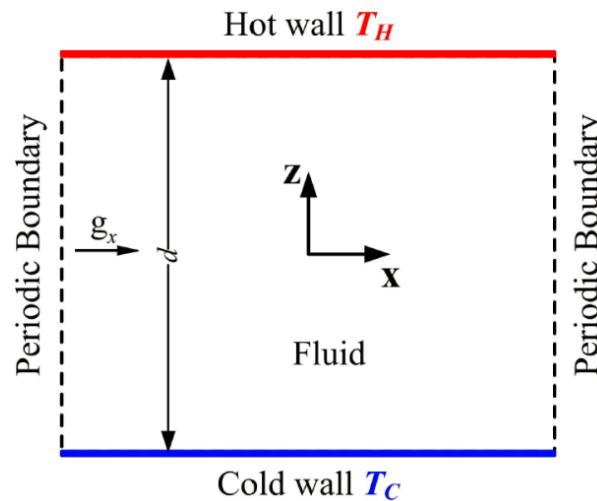
Flow between Cold-Hot walls:

— Li, Tang, Lei, Caswell & Karniadakis, J. Comput. Phys., 2014.

Temperature-dependent properties:



Coupling of flow and heat conduction:



Examples of Energy-conserving DPD

An easy way to compute the thermal conductivity:

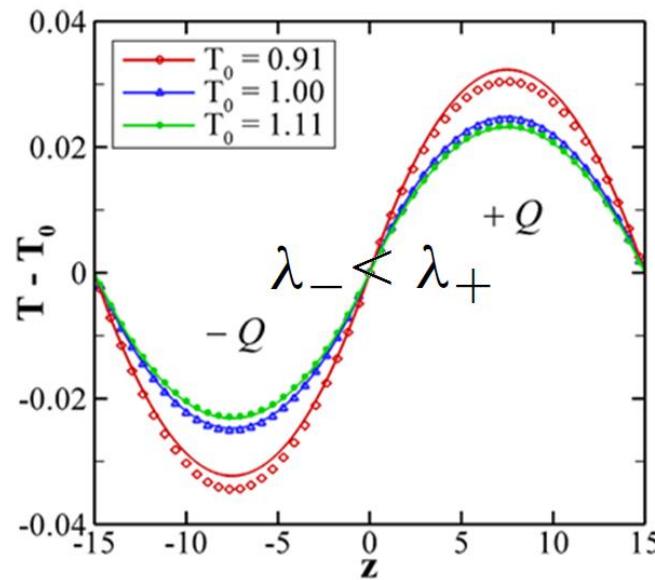
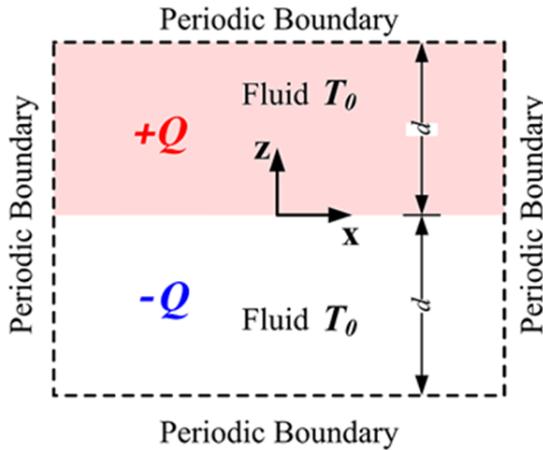
– Li, Tang, Lei, Caswell & Karniadakis, J. Comput. Phys., 2014.

The heat conduction of a fluid is governed by

$$\rho C_v \frac{\partial T}{\partial t} = \eta \nabla^2 T + \rho q \quad \text{For steady state} \quad \lambda \nabla^2 T = -Q \quad \longleftrightarrow \quad v \nabla^2 V = -g$$
$$\lambda = \eta / \rho C_v, \text{ and } Q = q / C_v$$

With a constant thermal diffusivity λ the steady state solution

$$T(z) = \frac{Qz}{2\lambda} (d - |z|) + T_0$$



When λ is temperature dependent:

$$\begin{aligned}\lambda(T_0) &= \frac{1}{2}(\lambda_+ + \lambda_-) \\ &= \frac{Q d^2}{16} \left(\frac{1}{T_{\max}} - \frac{1}{T_{\min}} \right)\end{aligned}$$

Outline

1. Single Particle DPD

Particle size: mono-size → multi-size

2. Many-body DPD

Quadratic EOS → Higher-order EOS

3. Energy conserving DPD

Isothermal system → Non-isothermal system

4. Smoothed DPD

Bottom-up approach → Top-down approach

5. Other DPD models

Mapping DPD units to Physical units

Bottom-up approach:

DPD is considered as coarse-graining of MD system

1. The mass of the DPD particle is N_m times the mass of MD particle.

$$m_{DPD} = N_m \cdot m_{MD}$$

2. The cut-off radius is determined by equating mass densities of MD and DPD systems.

$$\frac{m_{DPD} \cdot \rho_{DPD}}{r_C^3} = \frac{m_{MD} \cdot \rho_{MD}}{\sigma^3}$$

3. The time scale is determined by insisting that the shear viscosities of the DPD and MD fluids are the same.

$$t_{DPD} = \frac{\nu_{DPD}}{\nu_{MD}} \left(\frac{r_C}{\sigma} \right)^2 t_{MD}$$

DPD and Smoothed DPD

	DPD	Smoothed DPD
Major difference	Bottom-up approach	Top-down approach
	Coarse-graining force field governing DPD particles	Discretization of fluctuating Navier-Stokes equation
Inputs	Forms and coefficients for particle interactions, temperature, mesoscale heat friction	Equation of state, viscosity, temperature, thermal conductivity
Outputs	Equation of state, diffusivity, viscosity, thermal conductivity	As given
Advantages	1. No requirements in constitutive equation. 2. Good for complex materials and systems involving multicomponents.	Clear physical definition of parameters in Navier-Stokes equation
Disadvantages	1. No clear physical definition for the parameters. 2. Need to map DPD units to physical units based on output properties.	Must know the constitutive equation and properties of the system.

Equations of Smoothed DPD

Navier-Stokes equations in a Lagrangian framework:

$$\begin{aligned}\frac{d\rho}{dt} &= -\rho \nabla \cdot \mathbf{v} \\ \rho \frac{d\mathbf{v}}{dt} &= -\nabla P + \eta \nabla^2 \mathbf{v} + \left(\zeta + \frac{\eta}{3} \right) \nabla \nabla \cdot \mathbf{v} \\ T \rho \frac{ds}{dt} &= \phi + \kappa \nabla^2 T\end{aligned}$$

The transport coefficients are the shear and bulk viscosities η , ζ and the thermal conductivity κ . They are input parameters.

Discretize above equations using smoothed particle hydrodynamics (SPH) methodology, and introduce systematically thermal fluctuations via **GENERIC** framework, then we have the governing equations of smoothed DPD:

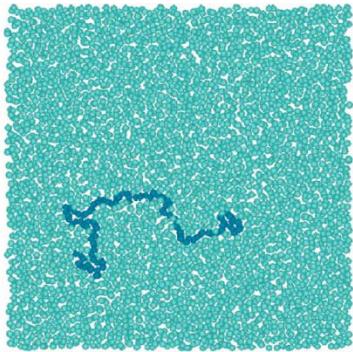
$$\begin{aligned}d\mathbf{r}_i &= \mathbf{v}_i dt & \mathbf{F}^C & & \mathbf{F}^D & & \mathbf{F}^R \\ m d\mathbf{v}_i &= \sum_j \left[\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right] F_{ij} \mathbf{r}_{ij} dt - \sum_j (1-d_{ij}) a_{ij} \mathbf{v}_{ij} dt - \sum_j (1-d_{ij}) \left(\frac{a_{ij}}{3} + b_{ij} \right) \mathbf{e}_{ij} \mathbf{e}_{ij} \cdot \mathbf{v}_{ij} dt + m d\tilde{\mathbf{v}}_i \\ T_i dS_i &= \frac{1}{2} \sum_j \left(1-d_{ij} - \frac{T_j}{T_i+T_j} \frac{k_B}{C_i} \right) \left[a_{ij} \mathbf{v}_{ij}^2 + \left(\frac{a_{ij}}{3} + b_{ij} \right) \times (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij})^2 \right] dt - \frac{2k_B}{m} \sum_j \left(\frac{T_i T_j}{T_i+T_j} \left(\frac{10}{3} a_{ij} + b_{ij} \right) \right) dt \\ &\quad - 2\kappa \sum_j \frac{F_{ij}}{d_i d_j} T_{ij} dt - 2\kappa \frac{k_B}{C_i} \sum_j \left(\frac{F_{ij}}{d_i d_j} T_j \right) dt + T_i d\tilde{S}_i.\end{aligned}$$

– Espanol and Revenga, Phys. Rev. E, 2003.

Examples of Smoothed DPD

Polymer chain in suspension:

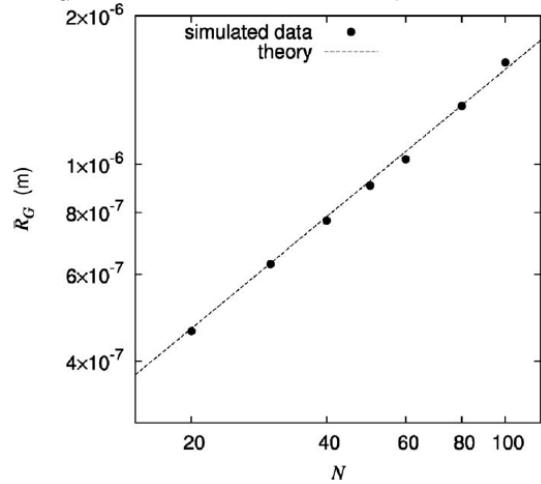
— Litvinov, Ellero, Hu & Adams, Phys. Rev. E, 2008.



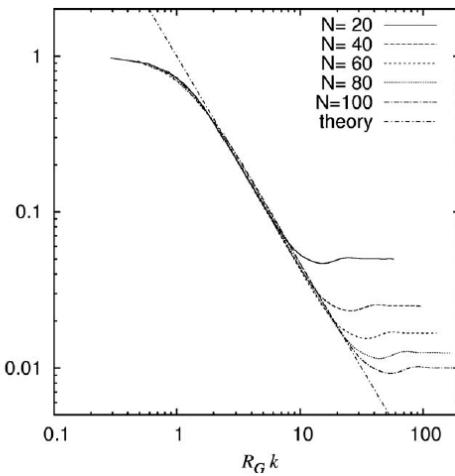
Solvent:
Newtonian fluid

Polymer chain:
Finitely Extendable Nonlinear
Elastic (FENE) springs

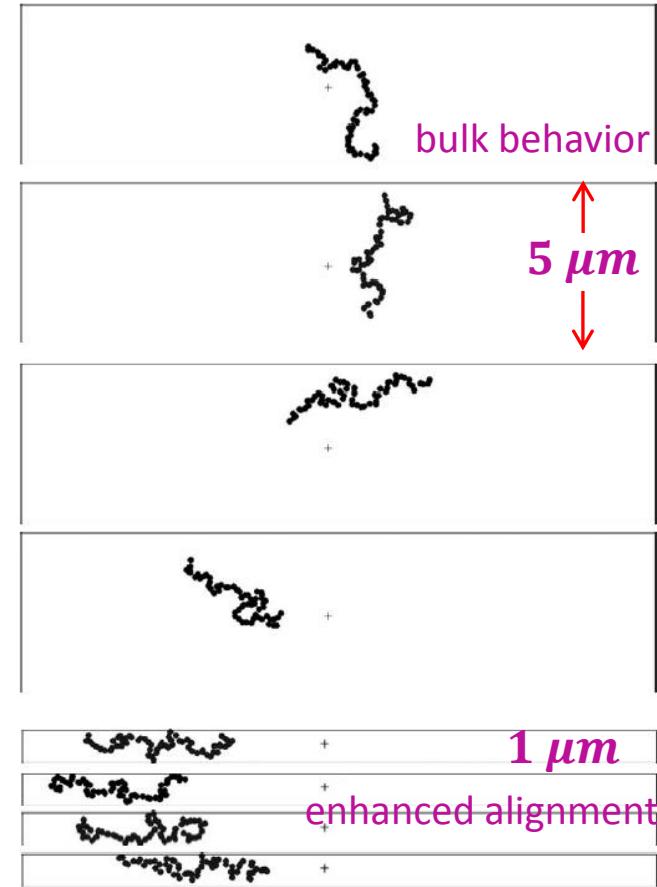
Scaling of the radius of gyration
 R_G for several chain lengths:



Static structure factor $\tilde{S}(k)$
 $= S(k)/S(0)$ versus $R_G k$:



Polymer conformations under
confinement:



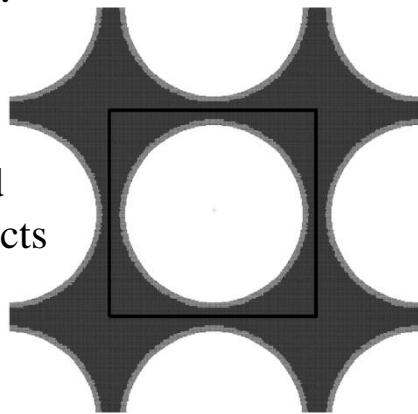
Examples of Smoothed DPD

Flow through porous media:

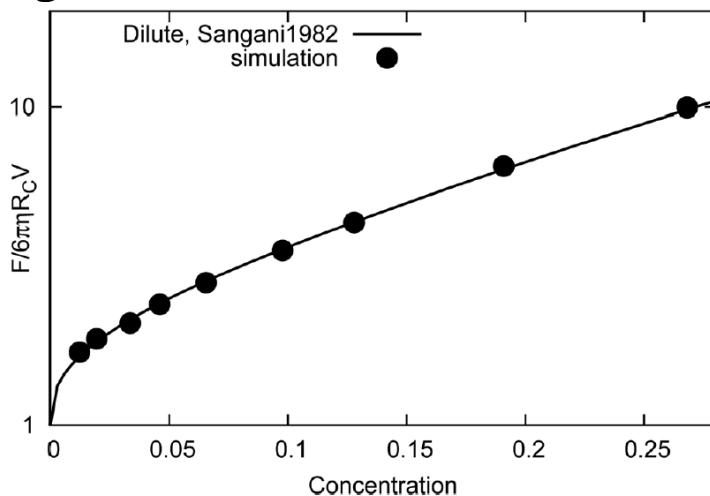
— Bian, Litvinov, Qian, Ellero & Adams,
Phys. Fluids, 2012.

Model:

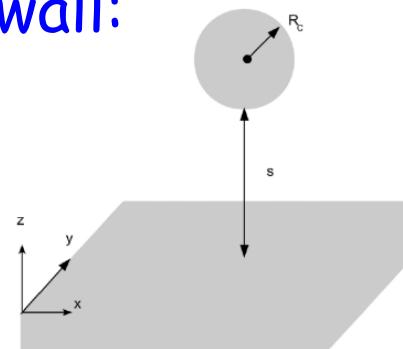
Periodic array of fixed
circular/spherical objects



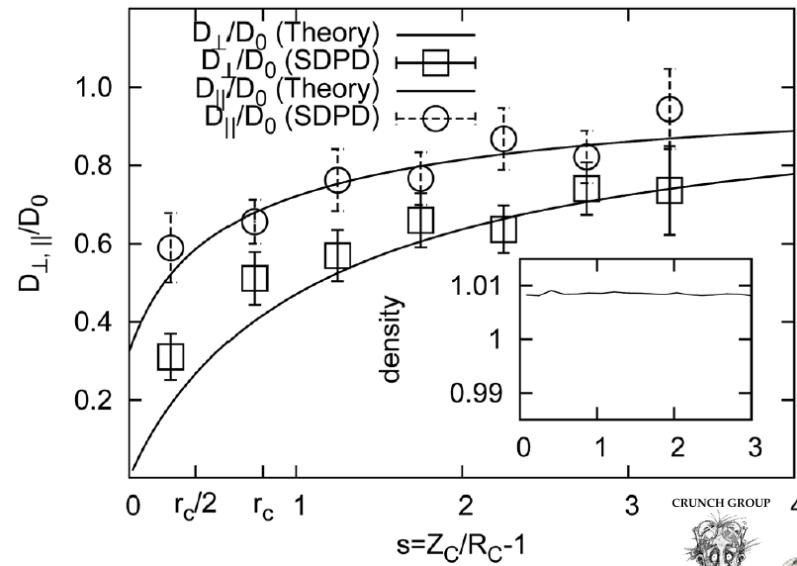
Three-dimensional dimensionless
drag coefficient:



A colloidal particle near a
rigid wall:



Diffusion coefficients perpendicular
and parallel to the wall:



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5. Other DPD models

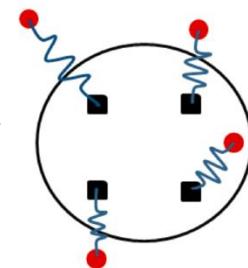
Other DPD models

1. Low-mass DPD model for an approximation of incompressible fluids.

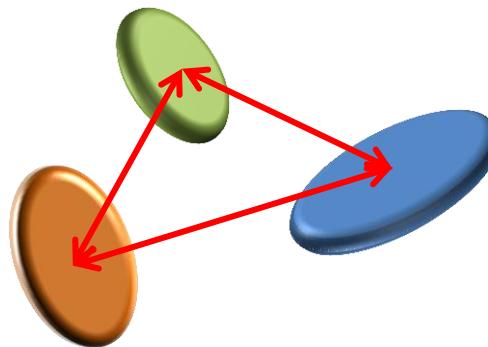
- Phan-Thien, N., Mai-Duy, N., Pan, D. and Khoo, B. C., Exponential-time differencing schemes for low-mass DPD systems. Computer Physics Communications, 2014. 185(1): 229-235.

2. Spring model for colloids in suspension.

- Phan-Thien, N., Mai-Duy, N. and Khoo, B.C., A spring model for suspended particles in dissipative particle dynamics. Journal of Rheology, 2014. 58(4): 839-867.



3. Anisotropic DPD particle (under development in CRUNCH group).



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